

RESEARCH ARTICLE

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Key Points:

- Anthropogenic nutrient enrichment alters the dynamics of microbial community on suspended sediment
- Microorganisms play an important role in modulating N cycle in suspended sediment
- Depolymerization of necromass contributes a control over the dynamics of N cycle

Supporting Information:

- Supporting Information S1
- Data Set S1
- Data Set S2
- Data Set S3

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Biomodulation of Nitrogen Cycle in Suspended Sediment

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Abstract Biogeochemical experiments and modeling were coupled to investigate how nutrient leaching to aquatic ecosystems changes the dynamics of microbial community on suspended sediment and how these changes modulate the nitrogen cycle. Mineral suspensions amended with inorganic nitrogen $(NH_4^+ \text{ and } NO_3^-)$ and inoculated with native sedimentary microbial strains were tested in a settling column under continuous water quality measurements. Experiments were used to calibrate and validate a kinetic model that explicitly described the chemical adsorption on minerals, aqueous complexation, gas dissolution, microbial metabolism, necromass dynamics, and microbial competition for limiting substrates. Modeling revealed that the interactions between microbial functional groups were highly nonlinear and highly sensitive to changes in nutrient and dissolved oxygen concentrations, showing shifts in regimes where a functional group became prevalent over the others. Our results suggested that necromass dynamics played a major role in sustaining microbial growth in low nutrient conditions and had an important control over the N cycle. The reaction network and model structure presented in this study provide a tool to analyze and predict the long-term nutrient dynamics of both natural and engineered aquatic ecosystems.

1. Introduction

Suspended particulate matter (SPM) has emerged as an important area of study for its role in geomorphology of coastal areas, estuaries, river banks, waterways, and harbors (e.g., Siviglia & Crosato, 2016; Toffolon, 2002) and in changing the quality of water and deposits (e.g., Bilotta & Brazier, 2008; Golterman et al., 1983; McCready et al., 2006). Over the years, a solid physical understanding of sediment dynamics has been established to model and predict sediment transport and deposition in natural waters (e.g., Green & Coco, 2014; Kranck, 1973; Maggi, 2005; McCave, 1984). However, this has mainly focused on hydrodynamic processes, with very little attention paid toward biological processes and ecological functions that modulate the dynamics of microbial community growing on suspended and deposited sediment, which, in turn, affects its transport and deposition (e.g., De Brouwer et al., 2000; Grossart et al., 2006; Kiørboe et al., 2002; Maggi, 2009; Montserrat et al., 2008; Tang & Maggi, 2016).

SPM never occurs as solely mineral. Mineral and biological phases normally coexist near-shore and in SPM because exchanges of nutrients, organic carbon, contaminants, and microorganisms between terrestrial and aquatic ecosystems happen at intense rates and high frequencies for multiple hydrometeorological, morphological, and geochemical causes (e.g., Callender & Hammond, 1982; Groffman & Bohlen, 1999; Gu et al., 2012; Wall et al., 2001). High heterogeneity in composition and the complexity of abiotic and biotic processes (e.g., chemicals, nutrients, and oxygen availability) make SPM a highly dynamic habitat capable of supporting a great variety of microbial strains in facilitative (mutualism and commensalism), competitive, or symbiotic interrelationship with one another (e.g., Dang & Lovell, 2016; Groffman & Bohlen, 1999; Horner-Devine et al., 2004); for instance, an oxygen gradient may develop within a SPM aggregate where the surface may be fully oxic and the inner core may be anoxic; hence, implying that both aerobic and anaerobic microorganisms can coexist and be active on the same aggregate (e.g., Ebrahimi & Or, 2015; Madigan et al., 2010). Each microbial population has its own ecological functions in the sedimentary microecosystem, and the interactions between them are complex and largely not understood. For example, phototrophic microalgae are the primary producers in the ecosystem, providing nutrients to heterotrophs (e.g., Brönmark & Hansson, 2005; Duarte & Cebrian, 1996) and oxygen to aerobic microorganisms; they may enhance, for example, mineralization of organic matter and nitrification (e.g., Pind et al., 1997; Rizzo, 1990; Wilson, 2006), which can then result





Figure 1. The experimental facility. (1) The settling column with (a) the flocculation section, (b) the diaphragm, and (c) the measuring section; (2) the oscillating grid used to provide isotropic and homogeneous mixing to the suspension; (3) motor and wheel that drive the grid; (4) water quality meter; (5) Cree light-emitting diode used to illuminate settling SPM; (6) optical fibers holder used to enhance illumination; (7) camera and magnification lens used to acquire images of free settling suspended particulate matter; and (8) microcontrolling system used to automate each component of the facility.

in positive feedback on the microalgae. However, how microbial composition changes against a changed environment is a complex problem that has been difficult to explain in its entirety. For instance, microorganisms colonizing and living on SPM (e.g., Grossart et al., 2006; Kiørboe et al., 2002, 2003; Kirchman, 2002) have been found to alter the chemistry, structure, and ambient characteristics of their habitat (e.g., size, surface irregularity, compactness, shear strength, permeability, stability, and sedimentation rate; Jones et al., 1994; Lubarsky et al., 2010; Maggi, 2015b; Maggi & Tang, 2015; Meadows et al., 2012; Tang & Maggi, 2016). Offsets in microbial ecological balance stemming from external perturbations such as changes in water temperature, nutrient concentrations, and presence of contaminants may therefore induce modification to the structure, transport, and deposition of SPM.

The aim of this study is to investigate the extent to which changes in nutrient supply can superpose changes in the native sedimentary microbial community, which in turn controls the N cycle. Focusing on the biogeochemical processes and ecological functions governed by NH_4^+ and $NO_3^$ leaching, we explore the microbial control on N fluxes and the effects of N leaching and dissolved oxygen on the microbial functional groups responsible for N cycle. Investigations were carried out by integrating experiments with biogeochemical modeling to describe the interactions between mineral, chemical, and biological phases in a sediment suspension. The experiment and model descriptions are presented in section 2, while the analyses of N cycle are presented in section 3.

2. Methods

2.1. Experiments

Three SPM suspension types (nutrient and biomass free NFBF, nutrient affected and biomass free, NABF, and nutrient and biomass affected, NABA) were tested for changes in SPM characteristic and water quality as a result of interactions between nutrients, minerals, and biological processes. While quantification of SPM physical characteristics was previously presented in Tang and Maggi (2016), this study focuses on the nutrient and mineral interactions relative to the NABF and NABA tests.

NABA tests were carried out by inoculating homogenous kaolinite mixtures with microbial strains present in natural sediment collected from the shallow water at the Blackwattle Bay, Sydney, NSW, Australia, on 1 January in 2015. NABA samples were prepared using 500 ml deionized water with added ammonium nitrate NH_4NO_3 and glucose $C_6H_{12}O_6$ as N and C sources at C:N ratio of 5:1. NABA samples were incubated for 21 days at 21°C at room atmosphere. NABF samples were prepared by mixing kaolinite with NH_4NO_3 dissolved in deionized water but were neither inoculated with microbial strains nor incubated. Three kaolinite concentrations C_K and two NH_4NO_3 concentrations were tested for each suspension type.

After incubation, samples were transferred into a settling column filled with 15 L of tap water. The chemical properties of tap water (i.e., NH_4^+ , NO_3^- , and CI^- concentrations, pH, and dissolved O_2) were measured prior to each test. The settling column (Figure 1) was equipped with an oscillating grid system to homogeneously mix the suspension and a water quality monitoring system to measure pH, dissolved O_2 , water temperature, turbidity, and NH_4^+ , NO_3^- , and CI^- concentrations every 30 s for approximately 15 hr at 21°C during each test. Detailed description of the settling column and experimental procedures was reported in Tang and Maggi (2015, 2016).

2.2. Reaction Network

Figure 2 shows the NH_4^+ and NO_3^- reaction pathways mediated by microorganisms, their adsorption, aqueous complexation, and gas exsolution. The microbial functional groups, reflecting those living in the estuarine







ecosystem, included (i) phototrophic bacteria B_{PHOTO} (e.g., cyanobacteria; Dworkin et al., 2006; Gottschalk, 1986; Raven, 2009); (ii) aerobic heterotrophic bacteria B_{HET} (e.g., pseudomonads and bacilli; *Mesonia*; Gottschalk, 1986; Wilson et al., 2010); (iii) nitrifying bacteria B_{NIT} (e.g., *Nitrosomonas, Nitrobacter*; Gottschalk, 1986; Raven, 2009; Van Kessel, 1977); (iv) denitrifying bacteria B_{DEN} (Van Kessel, 1977); and (v) dissimilatory nitrate reducing bacteria B_{DNR} (Van Kessel, 1977). A microbial metabolic reaction R_M was described as the sum of catabolic (energy producing) R_C and anabolic (biomass yielding) R_A reactions as (Rittmann & McCarty, 2001),

$$R_M = (1 - e)R_C + eR_A,\tag{1}$$

where *e* is the electrons (*e*⁻) fraction used for anabolism, $R_C = R_a - R_d$, and $R_A = R_s - R_d$, with R_a the *e*⁻ acceptor half-reaction, R_d the *e*⁻ donor half-reaction, and R_s the cell synthesis half-reaction. All microbial functional groups were described by dry mass stoichiometric composition of C₅H₇O₂N, though this may differ among microbial strains (e.g., Ebeling et al., 2006; Rittmann & McCarty, 2001).

 B_{PHOTO} uses H₂O as e^- donor to produce energy and releases H⁺ and O₂ as oxidization products (e.g., Kelly, 1971; Raven, 2009). Energy produced is used to reduce CO₂ (Kelly, 1971) and form glyceraldehyde-3-phosphate, which is used as the building block for cell synthesis (Rittmann & McCarty, 2001) in conjunction with either NH₄⁺ or NO₃⁻ as the N source. The NH₄⁺ and NO₃⁻ phototrophic assimilation (R1 and R2) were written as

R1 :
$$e_{R1}NH_4^+ + e_{R1}HCO_3^- + 4e_{R1}CO_2(aq) + e_{R1}H_2O(aq) \rightarrow 5e_{R1}O_2(aq) + e_{R1}B_{PHOTO}$$

R2 : $\frac{e_{R2}}{3}NO_3^- + \frac{e_{R2}}{3}H^+ + \frac{5e_{R2}}{3}CO_2(aq) + e_{R2}H_2O(aq) \rightarrow \frac{7e_{R2}}{3}O_2(aq) + \frac{e_{R2}}{3}B_{PHOTO}$

 B_{HET} assimilates either NH⁺₄ (R3) or NO⁻₃ (R4) to synthesis biomass by using C₆H₁₂O₆ and O₂ as the e^- donor and acceptor, respectively, (Gottschalk, 1986), resulting in

$$\begin{array}{rcl} \mathsf{R3} & : & \frac{6e_{\mathsf{R3}}}{5}\mathsf{NH}_4^+ + \mathsf{C}_6\mathsf{H}_{12}\mathsf{O}_6 + \frac{6e_{\mathsf{R3}}}{5}\mathsf{HCO}_3^- & \to & \left(6 - \frac{24e_{\mathsf{R3}}}{5}\right)\mathsf{CO}_2(\mathsf{aq}) + \left(6 - \frac{6e_{\mathsf{R3}}}{5}\right)\mathsf{H}_2\mathsf{O}(\mathsf{aq}) \\ & + 6(1 - e_{\mathsf{R3}})\mathsf{O}_2(\mathsf{aq}) & & + \frac{6e_{\mathsf{R3}}}{5}B_{\mathsf{HET}} \end{array}$$

$$\begin{array}{rcl} \mathsf{R4} & : & \frac{6e_{\mathsf{R4}}}{7}\mathsf{NO}_3^- + \mathsf{C}_6\mathsf{H}_{12}\mathsf{O}_6 + \frac{6e_{\mathsf{R4}}}{7}\mathsf{H}^+ & \to & \left(6 - \frac{30e_{\mathsf{R4}}}{7}\right)\mathsf{CO}_2(\mathsf{aq}) + \left(6 - \frac{18e_{\mathsf{R4}}}{7}\right)\mathsf{H}_2\mathsf{O}(\mathsf{aq}) \\ & + 6(1 - e_{\mathsf{R4}})\mathsf{O}_2(\mathsf{aq}) & & + \frac{6e_{\mathsf{R4}}}{7}B_{\mathsf{HET}} \end{array}$$

 B_{NIT} uses O_2 as the e^- acceptor to oxidize NH_4^+ to NO_3^- with a fraction of NH_4^+ being assimilated and CO_2 as the carbon source to build biomass (Ebeling et al., 2006; Rittmann & McCarty, 2001). This metabolic reaction (R5) was written as

$$R5 : \left(1 - \frac{e_{R5}}{8}\right) NH_4^+ + e_{R5}CO_2(aq) + \frac{e_{R5}}{4}HCO_3^- \rightarrow \left(1 - \frac{3e_{R5}}{8}\right) NO_3^- + \left(1 - \frac{5e_{R5}}{8}\right) H_2O(aq) + 2(1 - e_{R5})O_2(aq) + \left(2 - \frac{3e_{R5}}{4}\right) H^+ + \frac{e_{R5}}{4}B_{NIT}$$

 B_{DEN} is responsible for NO₃⁻ denitrification, whereas B_{DNR} performs dissimilatory NO₃⁻ reduction (DNR). Both B_{DEN} and B_{DNR} oxidize C₆H₁₂O₆ to CO₂ under anaerobic condition with NO₃⁻ as the e⁻ acceptor and a fraction of NO₃⁻ being assimilated. The metabolic reactions for denitrification (R6) and DNR (R7) were expressed as

$$\begin{array}{lll} \mathsf{R6} & : & \left(12 - \frac{78e_{\mathsf{R6}}}{7}\right)\mathsf{NO}_3^- + \mathsf{C}_6\mathsf{H}_{12}\mathsf{O}_6 + \frac{6e_{\mathsf{R6}}}{7}\mathsf{H}^+ & \rightarrow & 12(1 - e_{\mathsf{R6}})\mathsf{NO}_2^- + \left(6 - \frac{30e_{\mathsf{R6}}}{7}\right)\mathsf{CO}_2(\mathsf{aq}) \\ & & + \left(6 - \frac{18e_{\mathsf{R6}}}{7}\right)\mathsf{H}_2\mathsf{O}(\mathsf{aq}) + \frac{6e_{\mathsf{R6}}}{7}B_{\mathsf{DEN}} \\ \mathsf{R7} & : & \left(3 - \frac{15e_{\mathsf{R7}}}{7}\right)\mathsf{NO}_3^- + \mathsf{C}_6\mathsf{H}_{12}\mathsf{O}_6 + \left(6 - \frac{36e_{\mathsf{R7}}}{7}\right)\mathsf{H}^+ & \rightarrow & 3(1 - e_{\mathsf{R7}})\mathsf{NH}_4^+ + \left(6 - \frac{30e_{\mathsf{R7}}}{7}\right)\mathsf{CO}_2(\mathsf{aq}) \\ & & + \left(3 + \frac{3e_{\mathsf{R7}}}{7}\right)\mathsf{H}_2\mathsf{O}(\mathsf{aq}) + \frac{6e_{\mathsf{R7}}}{7}B_{\mathsf{DNR}} \end{array}$$

All functional groups are assumed to perish (R9) into biodegradable necromass (NEC) defined by the same chemical formula as living microorganisms ($C_5H_7O_2N$). NEC is then aerobically ammonified and depolymerized to NH₄⁺ and C₆H₁₂O₆ (R8) by B_{HET} as (e.g., Canfield et al., 2005; Riley et al., 2014)

$$\begin{aligned} \mathsf{R8}: \quad 2\mathsf{NEC} + \frac{(23 - 11e_{\mathsf{R8}})}{4}\mathsf{O}_2(\mathsf{aq}) + 5\mathsf{H}^+ & \to \quad (2 - e_{\mathsf{R8}})\mathsf{NH}_4^+ + (5 - 3e_{\mathsf{R8}})\mathsf{CO}_2(\mathsf{aq}) + \frac{1 + e_{\mathsf{R8}}}{2}\mathsf{H}_2\mathsf{O}(\mathsf{aq}) \\ & + \frac{5 - 2e_{\mathsf{R8}}}{6}\mathsf{C}_6\mathsf{H}_{12}\mathsf{O}_6 + e_{\mathsf{R8}}\mathcal{B}_{\mathsf{HET}} \end{aligned}$$

Finally, NH_4^+ and NO_3^- protection onto minerals (R10 and R11) as a result of adsorption, ion exchange, physical protection in mineral and organic matrix, and other uncharacterized processes (Riley et al., 2014) is considered to be not accessible for microbial consumption (Knicker & Hatcher, 1997). NH_4^+ and NO_3^- are also considered to be in equilibrium with NH_3 (aq) and HNO_3 (aq) (R12 and R13), whereas NH_3 (g), O_2 (g), and CO_2 (g) dissolution reactions (R16 to R18) are also accounted for explicitly. Derivations of Redox metabolic reactions R1 to R7 are reported in supporting information, and the kinetic parameters for reactions R9 to R18 are listed in Table 1.

2.3. Biogeochemical Modeling

The reaction network in Figure 2 was solved in the general purpose multiphase and multicomponent solver BRTSim-v2 based on Maggi (2015a). Equilibrium aqueous complexation and gaseous dissolution reactions were solved using the mass action law,

$$K_{\beta} = \prod_{R} [X_{R}]^{-x_{R}} \cdot \prod_{\rho} [X_{\rho}]^{x_{\rho}}, \qquad (2)$$

			Electron	Electron	Respiration	Carbon
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	Microbi	al metabolic kinetic reactions	donor	acceptor	type	source
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	R1	$\frac{1}{2}e_{R1}NH_{4}^{+} + 2e_{R1}H^{+} + \frac{5}{2}e_{R1}HCO_{3}^{-} \rightarrow \frac{5}{2}e_{R1}O_{2}(aq) + \frac{3}{2}e_{R1}H_{2}O(aq) + \frac{1}{2}e_{R1}B_{PHOTO}$	H_2O	CO ₂	Aerobic	CO ₂
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	R2	$\frac{5}{14}e_{R2}NO_{3}^{-} + \frac{15}{7}e_{R2}H^{+} + \frac{25}{14}e_{R2}HCO_{3}^{-} \rightarrow \frac{5}{2}e_{R2}O_{2}(aq) + \frac{5}{7}e_{R2}H_{2}O(aq) + \frac{5}{14}e_{R2}B_{PHOTO}$	H_2O	CO ₂	Aerobic	CO ₂
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	R3	$\frac{6}{5}e_{R3}NH_4^+ + C_6H_{12}O_6 + 6(1 - e_{R3})O_2(aq) \rightarrow (6 - \frac{24}{5}e_{R3})H^+ + (6 - 6e_{R3})HCO_3^- + \frac{18}{5}e_{R3}H_2O(aq) + \frac{6}{5}e_{R3}B_{HET}$	C ₆ H ₁₂ O ₆	02	Aerobic	C ₆ H ₁₂ O ₆
E (1 - $\frac{1}{2} q_{ex}) NH_{1}^{+} + 2(1 - e_{ex}) O_{2}(a t) + \frac{1}{2} q_{ex} H_{2}(O_{2} - (1 - \frac{3}{2} q_{ex}) H_{2}(0 t) + \frac{1}{2} q_{ex} H_{2}(O t t) + \frac{1}{2} q_{ex} H_{$	R4	$\frac{6}{7}e_{R4}NO_{3}^{-} + C_{6}H_{12}O_{6} + 6(1 - e_{R4})O_{2}(aq) \rightarrow (6 - \frac{36}{7}e_{R4})H^{+} + (6 - \frac{30}{7}e_{R4})HCO_{3}^{-} + \frac{12}{7}e_{R4}H_{2}O(aq) + \frac{6}{7}e_{R4}B_{HET}$	C ₆ H ₁₂ O ₆	02	Aerobic	$C_6H_{12}O_6$
Re $(-1)^{-2} g_{eqs} (NG_{7}^{2} + C_{1}^{4} + C_{1}^{0} - 2) (R_{1}^{2} + R_{1}^{0} + 1) (R_{1}^{2} - 2) (R_{2}^{0} + R_{1}^{0} + 1) (R_{1}^{0} - 1) (R_{1}^{0} - R_{1}^{0} + 1) (R_{1}^{0} - R_{1}^{0} - R_{1}^{0} + 1) (R_{1}^{0} - R_{1}^{0} - R_{1}^{0} - R_{1}^{0} - R_{1}^{0} - R_{1}^{0} - R_{1}$	R5	$(1 - \frac{1}{8}e_{R5})NH_4^+ + 2(1 - e_{R5})O_2(aq) + \frac{5}{4}e_{R5}HCO_3^- \rightarrow (1 - \frac{3}{8}e_{R5})NO_3^- + (2 - \frac{7}{4}e_{R5})H^+ + (1 + \frac{3}{8}e_{R5})H_2O(aq) + \frac{1}{4}e_{R5}B_{NIT}$	NH_4^+	02	Aerobic	CO ₂
R $(3 - \frac{1}{2} 4_{02}) N(2) + (4) N_{02} - 3(1 - e_{02}) NH_{1}^{2} + \frac{6}{2} e_{02} + 16C_{2} + (\frac{3}{2} - \frac{3}{2} e_{02}) HCO_{2} + (\frac{3}{2} - \frac{3}{2} - \frac{3}{2} + 16) HCO_{2} + (\frac{3}{2} - \frac{3}{2} - \frac{3}{2} + 16) HCO_{2} + (\frac{3}{2} - \frac{3}{2} - \frac{3}{2} + 16) HCO_{2} + (\frac{3}{2} - \frac{3}{2} - \frac{3}{2} + 16) HCO_{2} + (\frac{3}{2} - \frac{3}{2} + 16) $	R6	$(12 - \frac{79}{7}e_{R6})NO_3^- + C_6H_{12}O_6 \rightarrow 12(1 - e_{R6})NO_2^- + (6 - \frac{36}{7}e_{R6})H^+ + (6 - \frac{30}{7}e_{R6})HCO_3^- + \frac{12}{7}e_{R6}H_2O(aq) + \frac{6}{7}e_{R6}B_{DEN}$	C ₆ H ₁₂ O ₆	NO ⁻ 3	Anaerobic	C ₆ H ₁₂ O ₆
R8 NEC + $\frac{(2-1)^{-1}(1-1)}{2}O_2(\alpha) + 3e_{RB}H^+ + (\frac{2}{2} - \frac{2}{2}e_{RB})H_2(\alpha) - (2 - e_{RB})H_1^+ + (5 - 3e_{RB})H_2(\alpha) - (2 - e_{RB})H_1^+ + (\frac{2}{2} - \frac{2}{2}e_{RB})H_2(\alpha) - (2 - e_{RB})H_1^- + (2 - 2)A_1^ (2 - e_{RB})H_1^ (2 - e_{RB})H_1^-$	R7	$(3 - \frac{15}{7}e_{R7})NO_3^- + C_6H_{12}O_6 \rightarrow 3(1 - e_{R7})NH_4^+ + \frac{6}{7}e_{R7}H^+ + (6 - \frac{30}{7}e_{R7})HCO_3^- + (\frac{33}{7}e_{R7} - 3)H_2O(aq) + \frac{6}{7}e_{R7}B_{DNR}$	C ₆ H ₁₂ O ₆	NO ⁻ 3	Anaerobic	C ₆ H ₁₂ O ₆
	R8	$2NEC + \frac{(23-1)e_{RB}}{4}O_2(aq) + 3e_{RB}H^+ \\ + (\frac{9}{2} - \frac{7}{2}e_{RB})H_2O(aq) \\ \rightarrow (2 - e_{RB})NH_4^+ \\ + (5 - 3e_{RB})HCO_3^- \\ + \frac{(5 - 2e_{RB})e_{RB}}{6}C_6H_{12}O_6 \\ + e_{RB}B_{HET} \\ - \frac{1}{6}R_2O_6H_{12}O_6 \\ + \frac{1}{6}R_2O_6 \\ + \frac{1}{6}R_2O_6H_{12}O_6 \\ + \frac{1}{6}R_2O_6 \\ + \frac{1}{6}$	NEC	02	Aerobic	NEC
R1 $k_1 = 0$ k_1	Microb	al mortality reaction	δ (c ⁻¹)			
By $B_{x} \rightarrow NEC$ 2×10^{-64} Langmur adsorption kinetic reactions K_{x} q_{m} q_{0} Langmur adsorption kinetic reactions $(L^{m}m0)$ $(m0/g)$ $(m0/g)$ R10 $NH_{y}^{2}(q_{0}) \rightarrow NH_{y}^{2}(p)$ $(m0/g)$ $(m0/g)$ $(m0/g)$ R11 $NO_{y}^{2}(q_{0}) \rightarrow NH_{y}^{2}(p)$ $(M_{x} \rightarrow H^{2} + H^{2} + NH_{y}^{2}(q))$ $(1 \rightarrow 0^{2})$ 3.41×10^{-9b} R11 $NO_{y}^{2}(q_{0}) \rightarrow NH_{y}^{2}(p)$ $(1 \rightarrow 0^{2})$ 1.45×10^{-3b} 3.41×10^{-9b} R11 $NO_{y}^{2}(q_{0}) \rightarrow NH^{2}(q_{0})$ 1.45×10^{-3b} 3.41×10^{-9b} 3.41×10^{-9b} R12 $NH_{y}^{2} \rightarrow H^{2} \rightarrow NH^{2} + NO_{y}^{2}(q)$ 1.415^{-6} 1.45×10^{-3b} 3.41×10^{-9b} R13 $HNO_{y}^{2}(q) \rightarrow H^{2} + NO_{y}^{2}(q)$ 1.415^{-6} 1.415^{-6} 1.415^{-6} R13 $NH_{y}^{2}(q) \rightarrow H^{2} + NH_{y}^{2}(q)$ 1.30^{-6} 1.415^{-6} 1.415^{-6} R14 $OH^{2} + H^{2} + H_{y}^{2}(q) \rightarrow H^{2} + HCO_{y}^{2}$ 1.30^{-6} 1.413^{-6} 1.413^{-6} R14 $OH^{2} + H^{2} + H_{y}^{2}(q) \rightarrow H^{2} $						
Interface tends f_{11} q_{11} q_{11} q_{11} q_{11} q_{11} q_{11} q_{11} q_{11} q_{12} q_{11} q_{12} q_{11} q_{12} q_{11} q_{12} q_{11} q_{12}	R9	$B_x ightarrow \text{NEC}$	2×10^{-6a}			
R10 NH4 ⁺ ₄ (a) H1 ⁺ ₄ (b) 4433 ^b 1.05 × 10 ^{-3b} 1.06 × 10 ^{-4b} R11 NO ⁻ ₃ (aq) \rightarrow NO ⁻ ₃ (p) Iog(K _{aq}) Iog(K _{aq}) Iog(K _{aq}) Io6 × 10 ^{-4b} Equilibrium aqueous complexation reactions Equilibrium aqueous complexation reactions Iog(K _{aq}) Iog(K _{aq}) Io6 × 10 ^{-4b} R12 NH4 ⁺ ₄ \rightarrow H ⁺ $+$ NO ₃ R12 NH4 ⁺ ₄ \rightarrow H ⁺ $+$ NO ₃ Iog(K _{aq}) Iog(K _{aq}) Iog(K _{aq}) R13 NNO ₃ (aq) \rightarrow H ⁺ $+$ NO ₃ R1 O ⁺ \rightarrow H ⁺ \rightarrow H ₂ O(aq) Iog(K _{aq}) Iog(K _{aq}) R13 HNO ₃ (aq) \rightarrow H ⁺ \rightarrow H ₂ O(aq) H ⁺ $+$ H ₂ O(aq) Iog(K _q) Iog(K _q) R13 O ₂ (aq) \rightarrow H ⁺ \rightarrow H ₂ O(aq) H ⁺ $+$ H ₂ O(aq) Iog(K _q) Iog(K _q) R14 O ⁺ $+$ H ⁺ \rightarrow H ₂ O(aq) H ⁺ $+$ H ₂ O(aq) Iog(K _q) Iog(K _q) R16 NH ₃ (q) Iog(K _q) Iog(K _q) Iog(K _q) Iog(K _q) R17 O ₂ (aq) \rightarrow O ₂ (q) I ⁺ H ⁺ $+$ H ₂ O(aq) Iog(K _q) Iog(K _q) R17 O ₂ (aq) \rightarrow O ₂ (q) Iog(G) <	Langm	uir adsorption kinetic reactions	(L/mol)	q _m (mol/g)	q ₀ (mol/g)	
	R10	$NH^+_{A}(aq) \leftrightarrow NH^+_{A}(p)$	443.3 ^b	1.07×10^{-3b}	1.06×10^{-4b}	
Equilibrium aqueous complexation reactionsIog(K(aq))Iog(K(aq))Iog(K(aq))R12 $NH_4^+ \rightarrow H^+ \rightarrow NH_3(aq)$ at 21°Cat 21°CR13 $HO_3(aq) \rightarrow H^+ \rightarrow H_2O(aq)$ -9.24^c -9.37^d R14 $OH^- + H^+ \rightarrow H_2O(aq)$ 1.30^c 1.35^d R15 $CO_2(aq) + H^+ O(aq)$ $H^+ + HCO_3^ 1.30^c$ 1.31^d R16 $OH^- + H^+ \rightarrow H_2O(aq)$ $H^+ + HCO_3^ -6.37^d$ -6.37^d R15 $CO_2(aq) + H_2O(aq)$ $H^+ + HCO_3^ -6.37^d$ -6.37^d R16 $NH_3(aq)$ $H^+ + HCO_3^ 1.30^c$ $1.31^g d$ R17 $O_2(aq) \rightarrow O_2(q)$ 1.30^c 2.30^c 2.87^d R18 $CO_2(q) + H_2O(aq) \rightarrow H^+ + HCO_3^ -7.38^f$ -7.28^f	R11	$NO_{3}^{-}(aq) \leftrightarrow NO_{3}^{-}(p)$	1608.4 ^b	1.45×10^{-3b}	3.41×10^{-9b}	
R12 $NH_4^+ \leftrightarrow H^+ + NH_3(aq)$ -9.24^c -9.37^d R13 $HNO_3(aq) \leftrightarrow H^+ + NO_3^ 1.30^c$ 1.35^d R14 $OH^- + H^+ \leftrightarrow H_2O(aq)$ $1.3.99^c$ 14.13^d R15 $CO_2(aq) + H_2O(aq) \leftrightarrow H^+ + HCO_3^ -6.37^d$ -6.37^d R16 $NH_3(q) \leftrightarrow NH_3(aq)$ $H^+ + HCO_3^ Ia_1 S^2 C_2^- C_3^- C_3^-$	Equilib	ium aqueous complexation reactions	log(K _(aq)) at 25°C	log(K _(aq)) at 21°C		
R13 $HNO_3(aq) \leftrightarrow H^+ + NO_3^{-}$ $I.3C$ $I.35^{d}$ R14 $OH^- + H^+ \leftrightarrow H_2O(aq)$ $I.13^{d}$ $I.3.99^{c}$ $I.4.13^{d}$ R15 $CO_2(aq) + H_2O(aq) \leftrightarrow H^+ + HCO_3^{-}$ $I.3.99^{c}$ $I.4.13^{d}$ R15 $CO_2(aq) + H_2O(aq) \leftrightarrow H^+ + HCO_3^{-}$ $I.3.99^{c}$ $I.4.13^{d}$ R16 $NH_3(q) \leftrightarrow NH_3(aq)$ $I.3.96^{c}$ $I.4.13^{d}$ R16 $NH_3(q) \leftrightarrow NH_3(aq)$ $I.3.96^{c}$ $I.3.96^{c}$ $I.80^{c}$ R17 $O_2(aq) \leftrightarrow O_2(q)$ $I.80^{c}$ $I.80^{c}$ $I.80^{c}$ $I.80^{c}$ R17 $O_2(aq) \leftrightarrow O_2(q)$ $I.4.1 \leftrightarrow HCO_3^{-}$ $I.80^{c}$ $I.80^{c}$ $I.80^{c}$ R18 $CO_2(g) + H_2O(aq) \leftrightarrow H^+ + HCO_3^{-}$ $I.7.80^{c}$ $I.7.80^{c}$ $I.7.80^{c}$ $I.7.80^{c}$	R12	$NH^+_4 \leftrightarrow H^+ + NH_3(aq)$	-9.24 ^c	-9.37 ^d		
R14 $OH^- + H^+ \leftrightarrow H_2O(aq)$ 13.99c 14.13 ^d R15 $CO_2(aq) + H_2O(aq) \leftrightarrow H^+ + HCO_3^ -6.34^c$ -6.37^d Equilibrium gas dissolution reactions $Igg(K_{(g)})$ $Igg(K_{(g)})$ $Igg(K_{(g)})$ R16 $NH_3(g) \leftrightarrow NH_3(aq)$ $I.80^c$ $I.80^c$ $I.88^d$ R17 $O_2(aq) \leftrightarrow O_2(q)$ $I.80^c$ $I.88^d$ $I.80^c$ $I.88^d$ R17 $O_2(aq) \leftrightarrow O_2(q)$ $I.4+HCO_3^ I.80^c$ $I.88^d$ $I.88^d$ R18 $CO_2(g) + H_2O(aq) \leftrightarrow H^+ + HCO_3^ I.80^c$ $I.80^c$ $I.88^d$ $I.81^c$ <t< td=""><td>R13</td><td>$HNO_3(aq) \leftrightarrow H^+ + NO_3^-$</td><td>1.30^c</td><td>1.35^d</td><td></td><td></td></t<>	R13	$HNO_3(aq) \leftrightarrow H^+ + NO_3^-$	1.30 ^c	1.35 ^d		
R15 $CO_2(aq) + H_2O(aq) \leftrightarrow H^+ + HCO_3^ -6.34^c$ -6.37^d Equilibrium gas dissolution reactions $log(K_{(g)})$ $log(K_{(g)})$ R16 NH_3(g) $\leftrightarrow NH_3(aq)$ 1.80^c 1.80^c 1.88^d R17 $O_2(aq) \leftrightarrow O_2(g)$ 1.80^c 1.88^d 2.90^c 2.87^d R18 $CO_2(g) + H_2O(aq) \leftrightarrow H^+ + HCO_3^ -7.81^c$ -7.81^c -7.78^d	R14	$OH^- + H^+ \leftrightarrow H_2O(aq)$	13.99 ^c	14.13 ^d		
Equilibrium gas dissolution reactions $log(K_{(g)})$ $log(K_{(g)})$ R16NH3(g) \leftrightarrow NH3(aq)at 21°Cat 21°CR17 $O_2(aq) \leftrightarrow O_2(g)$ 1.88d1.88dR17 $O_2(aq) \leftrightarrow O_2(g)$ 2.90°2.87dR18 $CO_2(g) + H_2O(aq) \leftrightarrow H^+ + HCO_3^ -7.81^c$ -7.78^d	R15	$CO_2(aq) + H_2O(aq) \leftrightarrow H^+ + HCO_3^-$	-6.34 ^c	-6.37 ^d		
R16 $NH_3(g) \leftrightarrow NH_3(aq)$ at 21°CR17 $O_2(aq) \leftrightarrow O_2(g)$ 1.80^c R17 $O_2(aq) \leftrightarrow O_2(g)$ 2.87^d R18 $CO_2(g) + H_2O(aq) \leftrightarrow H^+ + HCO_3^ -7.78^d$	Equilib	ium gas dissolution reactions	$\log(K_{(g)})$	$\log(k_{(g)})$		
R16 $NH_3(g) \leftrightarrow NH_3(aq)$ 1.80 ^c 1.88 ^d R17 $O_2(aq) \leftrightarrow O_2(g)$ 2.90 ^c 2.87 ^d R18 $CO_2(g) + H_2O(aq) \leftrightarrow H^+ + HCO_3^ -7.81^c$ -7.78^d			at 25°C	at 21°C		
R17 $O_2(aq) \leftrightarrow O_2(g)$ 2.87^d R18 $CO_2(g) + H_2O(aq) \leftrightarrow H^+ + HCO_3^ -7.81^c$ -7.78^d	R16	$NH_3(g) \leftrightarrow NH_3(aq)$	1.80 ^c	1.88 ^d		
$ \begin{array}{ccc} R18 & CO_2(g) + H_2O(aq) \leftrightarrow H^+ + HCO_3^- \\ \end{array} \\ \end{array} \qquad \qquad -7.81^c & -7.78^d \end{array} $	R17	$O_2(aq) \leftrightarrow O_2(g)$	2.90 ^c	2.87 ^d		
	R18	$CO_2(g) + H_2O(aq) \leftrightarrow H^+ + HCO_3^-$	-7.81 ^c	-7.78 ^d		



where K_{β} is the equilibrium constant in phase β (either aqueous or gaseous) reported in the EQ3/6 database (Wolery, 1992), $[X_R]$ and $[X_P]$ are the concentrations [mol/L] (for aqueous phase) or partial pressure fraction [–] (for gaseous phase) of reactants X_R and products X_P , respectively, while, x_R and x_P are their corresponding stoichiometric numbers.

 NH_4^+ and NO_3^- protection was described using Langmuir adsorption kinetics (e.g., Atkins & De Paula, 2005; Langmuir, 1918) as

$$\frac{d[X(p)]}{dt} = k_a[X(aq)](Q_m - [X(p)]) - k_d[X(p)],$$
(3)

where [X(p)] and [X(aq)] are the concentrations [mol/L] of chemical X in protected (p) and aqueous (aq) phases, respectively, k_a and k_d are the adsorption and desorption rate constants, respectively, and $Q_m = q_m C_K$ includes the maximum adsorption capacity q_m [mol of X adsorbed/g of mineral] and the mineral concentration C_K [g/L]. Note that at equilibrium (d[X(p)]/dt = 0), $K_L = k_a/k_d = [X(p)]/([X(aq)](Q_m - [X(p)]))$ is the Langmuir equilibrium constant.

Microbial metabolism was described by Michaelis-Menten-Monod kinetics with reaction rate r written as (Maggi, 2015a)

$$r = \hat{\mu} \cdot \frac{[\mathcal{B}_{x}]}{Y} \cdot \prod_{p} [X_{p}]^{n_{p}} \cdot \prod_{i} \frac{[X_{i}]}{[X_{i}] + \mathcal{K}_{\mathcal{M}_{i}} \left(1 + \sum_{j} \frac{[X_{j}]}{\mathcal{K}_{\mathcal{M}_{j}}}\right)} \cdot \prod_{m} \frac{\mathcal{K}_{\mathcal{H}_{m}}}{\mathcal{K}_{\mathcal{H}_{m}} + [X_{m}]}, \tag{4}$$

where $\hat{\mu}$ is the maximum specific biomass growth rate, $[B_x]$ is the concentration of microbial functional group B_x , and Y is the biomass yield. The third factor on the right-hand side describes the n_p -order kinetic product for reactant X_p and $n_p = \{1, 2, 3, ..., n\}$ for first, second, third, and n-order kinetics, respectively. The fourth factor on the right-hand side expresses the Michaelis-Menten-Monod kinetic terms for reactant X_i with K_{M_i} its half-saturation concentration. The term in the parenthesis describes the competitive substrate consumption between reactants X_i and X_j with K_{M_j} its half-saturation concentration. The last term on the right-hand side expresses a decrease in r due to the presence of an inhibitor X_m with inhibition constant K_{H_m} . The rate of change in the concentration of a generic chemical X_n was then written as

$$\frac{\mathbf{I}[\mathbf{X}_n]}{\mathrm{d}t} = \sum_i (x_{n_i} \cdot r_i),\tag{5}$$

with x_{n_i} as the stoichiometric number of X_n in reaction r_i . The rate of change in $[B_x]$ was described by Monod kinetics as (Monod, 1949),

C

$$\frac{\mathsf{d}[B_x]}{\mathsf{d}t} = \sum_i Y_i r_i - \delta[B_x],\tag{6}$$

where the microbial mortality rate $\delta = 2 \times 10^{-6} \text{ s}^{-1}$ was assumed after Servais et al. (1985) and Billen et al. (1990) for all functional groups.

Microbial competition for the same substrate was accounted for by K_M in equation (4). All reactions involving $O_2(aq)$ and HCO_3^- consumption were assumed to have the same K_M values. Competitive substrate consumption relative to NH_4^+ and NO_3^- was included for N assimilation by B_{PHOTO} and B_{HET} (R1 to R4). pH inhibition was explicitly accounted for with $K_M = 1 \times 10^{-9}$ mol/L for low [H⁺] and with $K_H = 1 \times 10^{-5}$ mol/L for high [H⁺] (Boon & Laudelout, 1962; Saleh-Lakha et al., 2009). O_2 inhibition on anaerobic reactions (R6 and R7) was also explicitly included. Finally, $C_6H_{12}O_6$ inhibition on depolymerization and ammonification (R8) was considered here because B_{HET} is expected to have higher preference for simple (i.e., $C_6H_{12}O_6$) over complex C sources such as necromass (Goldman & Dennett, 1991).

2.4. Parameter Estimation

Langmuir kinetic parameters k_a , k_d , and q_m in equation (3), and the initial N ions protected in one gram of minerals q_0 were calibrated for NH⁺₄ and NO⁻₃ adsorption against NABF experiments. The remaining unknowns (i.e., $\hat{\mu}_s$, K_M , K_H , e, and initial biomass concentrations $[B_x]_0$) were estimated against NABA experiment conducted at $[NH_4NO_3] = 6 \text{ mM}$, $[C_6H_{12}O_6] = 11.6 \text{ mM}$, and $C_K = 3 \text{ g/L}$; in total, 192 data points of NH⁺₄, NO⁻₃, pH, and O₂(aq) acquired during the column testing were used for calibration. Model parameters were estimated with Model-Independent Parameter Estimation and Uncertainty Analysis (Doherty, 2005), which uses the Gauss-Marquardt-Levenberg algorithm (Levenberg, 1944) to minimize the errors between modeled and observed data.

The model structure and estimated parameters were validated against independent NABA experiments with $[NH_4NO_3]$, $[C_6H_{12}O_6]$ and C_K different from those for estimation. Goodness of fit was measured using the correlation coefficient (*R*), the normalized root-mean-square error (NRMSE), Nash-Sutcliffe efficiency (NSE) (Nash & Sutcliffe, 1970), index of agreement (IA) (e.g., Willmott, 1982; Willmott et al., 1985), and percent bias (PBIAS) (Sorooshian et al., 1993),

$$R = \frac{\text{cov}(c, o)}{\sigma_c \sigma_o}, \quad \text{with} \quad -1 \le R \le 1,$$
 (7a)

$$NRMSE = \frac{\sqrt{\frac{1}{n_o} \sum_{i=1}^{n_o} (c_i - o_i)^2}}{\max\{o\} - \min\{o\}} \times 100, \quad \text{with} \quad 0 \le NRMSE < \infty, \quad (7b)$$

$$NSE = 1 - \frac{\sum_{i=1}^{n_o} (o_i - c_i)^2}{\sum_{i=1}^{n_o} (o_i - \bar{o})^2}, \quad \text{with} \quad -\infty < NSE \le 1, \quad (7c)$$

$$IA = 1 - \frac{\sum_{i=1}^{n_0} (o_i - c_i)^2}{\sum_{i=1}^{n_0} (|c_i - \bar{o}| + |o_i - \bar{o}|)^2}, \quad \text{with} \quad 0 \le IA \le 1,$$
(7d)

$$\mathsf{PBIAS} = \frac{\sum_{i=1}^{n_o} (c_i - o_i)}{\sum_{i=1}^{n_o} o_i} \times 100, \qquad \text{with} \quad -\infty < \mathsf{PBIAS} < \infty, \tag{7e}$$

where *c* and *o* are the calculated and observed values of the state variables, respectively, n_o is the number of observations, σ_c and σ_o are the corresponding standard deviations, and \bar{o} is the average of *o*. Modeled values match observations when $R \rightarrow 1$, NRMSE $\rightarrow 0\%$, NSE $\rightarrow 1$, IA $\rightarrow 1$, and PBIAS $\rightarrow 0\%$. NSE = 0 implies that *c* is as accurate as \bar{o} , while, NSE < 0 signifies that \bar{o} is a better prediction than the model. PBIAS measures model overestimation (PBIAS > 0) or underestimation (PBIAS < 0). A validation test was considered satisfactory if conditions $R \ge 0.8$, NRMSE $\le 15\%$, NSE ≥ 0 , IA ≥ 0.8 , and $-15\% \le PBIAS \le 15\%$ were satisfied and signified that model structure and parameter uncertainty were suitable to describe that experiment.

2.5. Analyses of Nutrient Leaching and Dissolved Oxygen Content

The model was used to investigate the effects of NH⁴₄ and NO³₃ leaching on microbial dynamics at steady state. A total of 400 simulations were run for leaching rates $R_{\rm NH^4_4}$ and $R_{\rm NO^3_3}$ between 5 × 10⁻⁴ and 5 × 10⁻² mol · L⁻¹ · day⁻¹. All simulations were initialized with equal biomass across all functional groups. C:N ratio was kept at 8:1 as commonly found in estuarine sediment (Matson & Brinson, 1990), while C_K was kept at 0.1 g/L. Microbial metabolism was assumed not to be limited by [H⁺], [HCO³₃], and [O₂(aq)], which were assumed to be continuously recharged in natural aquatic ecosystem through various buffering processes not explicitly included in the model; hence, pH was kept at approximately 7 and [HCO³₃] was maintained at approximately 6 × 10⁻⁵ mol/L so as to be in equilibrium with pH 7 and atmospheric CO₂(g). The concentration of dissolved oxygen was maintained at 2.87 × 10⁻⁴ mol/L, which corresponds to 100% saturation at 21°C. Simulations were run until the ecosystem reached the steady state.

Simulations of $R_{NH_4^+}$ and $R_{NO_3^-}$ between 5×10^{-4} and 5×10^{-2} mol $\cdot L^{-1} \cdot day^{-1}$ with $R_{NH_4^+}$: $R_{NO_3^-} = 1:1$ were also conducted at different O₂(aq) saturations to investigate the effects of O₂ on N fluxes. All simulations were conducted with the same boundary and initial conditions as above.

3. Results

3.1. Analysis of Kinetic Parameters

Estimated Langmuir parameters for NH_4^+ and NO_3^- adsorption on kaolinite (Table 1) matched relatively well those reported in the literature (e.g., Cengeloglu et al., 2006; Copcia et al., 2010; Li & Bowman, 2001). Experimentally determined kinetic parameters relative to reactions R1 to R8 are listed in Table 2. The maximum specific biomass growth rate $\hat{\mu}$ ranged from about 1×10^{-5} (R3) to 4×10^{-4} s⁻¹ (R8). The biomass yield *Y* was the highest in phototrophic NH_4^+ assimilation in R1 and nitrification in R5 and the lowest in necromass depolymerization in R8. No correlation was found between $\hat{\mu}$ and *Y* (i.e., R = -0.46). K_M values spanned across a wide range from 1.5×10^{-6} to 5.7×10^{-2} mol/L (Table 2). The $O_2(aq)$ inhibition constant K_H in denitrification in R6 was higher than in DNR in R7, implying that B_{DEN} had higher tolerance to $O_2(aq)$ than B_{DNR} . The reaction

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Table 2 Summary of Estimated Parameters for Microbial Metab	oolic Reactions I	81 to R8							
					Reacti	ons			
Parameter values		R1	R2	R3	R4	R5	R6	R7	R8
Maximum specific biomass growth rate $\hat{\mu}$ (×10 ⁻⁵ s ⁻¹		2.661	10.794	1.000	12.480	16.491	5.573	4.352	40.778
Fraction of electron used for cell synthesis <i>e</i> (-)		1.0	1.0	0.115	0.081	0.149	0.119	0.119	0.046
Biomass yield Y (mol of $B_{\rm X}$ /mol of C source)		0.25	0.20	0.138	0.069	0.25	0.102	0.102	0.023
Biomass yield Y (g of dry B_{x}/g of C source)		0.6422	0.5138	0.0866	0.044	0.6422	0.064	0.064	0.023
Michaelis-Menten constant $K_{\mathcal{M}}$ (mol/L)	NH^+_4	3.007×10^{-3a}		1.405×10^{-5b}		3.554×10^{-2}	Ι		Ι
	NO ¹	I	5.288×10^{-2a}	I	1.281×10^{-2b}	I	4.636×10^{-3}	6.153×10^{-4}	Ι
	C ₆ H ₁₂ O ₆			5.719×10^{-2c}	5.162×10^{-3c}		1.470×10^{-3}	8.096×10^{-4}	Ι
	$O_2(aq)$		I	6.567×10^{-5}	6.567×10^{-5}	6.567×10^{-5}	I		6.567×10^{-5}
	HCO ⁻	1.971×10^{-5}	1.971×10^{-5}	I	Ι	1.971×10^{-5}	I	I	Ι
	NEC						I		1.507×10^{-6}
	+ H	1×10^{-9}	1×10^{-9}	1×10^{-9}	1×10^{-9}	1×10^{-9}	1×10^{-9}	1×10^{-9}	1×10^{-9}
Inhibition constant K_H (mol/L)	Ŧ	1×10^{-5}	1×10^{-5}	1×10^{-5}	1×10^{-5}	1×10^{-5}	1×10^{-5}	1×10^{-5}	1×10^{-5}
	$O_2(aq)$			I			1.907×10^{-3}	1.510×10^{-4}	Ι
	C ₆ H ₁₂ O ₆	I	I	I		I	I	I	6.175×10^{-5}
a Competition term was included in R1 and R2 to acct substrate consumption between NH_4^+ and NO_3^ c Cc	ount for compe ompetition terr	titive substrate c m was included ii	onsumption bet: n R3 and R4 to a	ween NH ⁺ and N ccount for comp	VO ⁻ . ^b Competiti etitive substrate e	ion term was incl consumption of	luded in R3 and C ₆ H ₁₂ O ₆ .	R4 to account fo	r competitive





Figure 3. Comparison between experimental measurements and modeled results for (a) $[NH_4^+]$, (b) $[NO_3^-]$, (c) pH, (d) the net oxygen consumption $[O_2(aq)]_C$, and microbial concentrations for (f) phototrophic bacteria B_{PHOTO} , (g) heterotrophic bacteria B_{HET} , (h) nitrifying bacteria B_{NIT} , (i) denitrifying bacteria B_{DEN} , (j) dissimilatory nitrate reducing bacteria B_{DNR} , and (k) necromass (NEC). Note that the incubation phase was plotted in a time scale of days, while the column testing phase was plotted in a time scale of hours.

velocity of R8 was reduced by more than 50% when $[C_6H_{12}O_6] > 6.18 \times 10^{-5}$ mol/L, thus accounting for B_{HET} to have higher preference for simpler monosaccharide as a C source than NEC.

Qualitatively, the model matched relatively well the $[NH_4^+]$, $[NO_3^-]$, pH, and the net O_2 consumption $[O_2(aq)]_C$ measured during column testing (Figure 3, first column). During the 21 day incubation, $[NH_4^+]$ initially decreased due to adsorption onto kaolinite and was nearly constant afterward because NH_4^+ consumed by B_{NIT} in R5 (contributing about 99%) was balanced by its production in reactions R7 and R8 (contributing about 98% and 2%, respectively; Figure 3a). NO_3^- decreased sharply at the beginning of incubation due to adsorption and gradually later on because of consumption by B_{DEN} (68%), B_{DNR} (32%), and B_{HET} and B_{PHOTO} (contributing less than 0.02%) (Figure 3b). NO_3^- produced by B_{NIT} was unable to sustain uptake by other microbial functional groups. After the initial phase, pH stabilized at about 5 by the end of incubation (Figure 3c). The net oxygen consumption $[O_2(aq)]_C$ increased during incubation, implying that the ecosystem had more intense aerobic respiration than photosynthesis (Figure 3d).

All microbial functional groups showed an initial increase in their concentrations (Figure 3, right column) and reached a maximum between day 7 and 14 of the incubation period. In contrast, [NEC] increased steadily. The biomass fraction in each functional group fluctuated during the whole test depending on substrate availability and environmental conditions (e.g., pH, O₂(aq)).

3.2. Goodness-of-Fit Analyses

Analyses of goodness of fit show that the modeled concentrations in Figure 3 matched relatively well the experimental $[NH_4^+]$, $[NO_3^-]$, pH, and $[O_2(aq)]_C$, with $R \ge 0.9$, NRMSE $\le 14\%$, NSE ≥ 0.8 , IA ≥ 0.95 , and $-0.5\% \le$ PBIAS $\le 4\%$ (Figure 4, cells marked with red asterisk).

Validation tests conducted against independent experiments at different [NH₄NO₃] and C_{κ} (Figure 4) also showed relatively good agreement, with 100% state variables having $R \ge 0.8$, 95% having NRMSE $\le 15\%$,





Figure 4. Goodness-of-fit analyses of the modeled against experimental $[NH_4^+]$, $[NO_3^-]$, pH, and the net oxygen consumption $[O_2(aq)]_C$ using (a) correlation coefficient (*R*), (b) normalized root-mean-square error (NRMSE), (c) Nash-Sutcliffe efficiency (NSE), (d) index of agreement (IA), and (e) percent bias (PBIAS). The red asterisk indicates calibration set and the green dot represents validation tests that passed the goodness-of-fit benchmark analyses. "+" and "-" signs indicate positive and negative values in *R* and PBIAS tests, respectively. Note that kaolinite concentration C_K and $[NH_4NO_3]$ values plotted correspond to the initial concentrations in incubation.

100% having NSE \geq 0, 100% having IA \leq 0.8, and 80% having $-15\% \leq$ PBIAS \leq 15%; in average, 95% of validation tests passed the benchmark values stated in section 2.4.

3.3. Effect of Nutrient Leaching

The effect of nutrient leaching on the steady state N dynamics and microbial community was investigated using model parameters reported in section 3.1 with pH, $[O_2(aq)]$, and $[CO_2(aq)]$ kept constant at optimum values for microbial growth.

At steady state, the total living biomass B_{TOT} generally increased with increasing $R_{NO_3^-}$, but it decreased when $R_{NH_4^+}$ was greater than 2×10^{-2} mol·L⁻¹ · day⁻¹ (Figure 5a). In contrast, the necromass NEC (not shown here) increased linearly with increasing nutrient leaching rates. Among all microbial groups, B_{PHOTO} constituted 92% of B_{TOT} (Figure 5b), while B_{HET} contributed less than 8% at $R_{NH_4^+} < 2 \times 10^{-2}$ mol/L (Figure 5c) and B_{DNR} survived only when leaching rates were greater than 2×10^{-2} mol·L⁻¹ · day⁻¹ (Figure 5d). B_{NIT} and B_{DEN} were completely outcompeted by the other functional groups at steady state, as opposed to the transient incubation phase (Figures 3g and 3h) where they were the most abundant.

In all nutrient leaching scenarios, more than 99% of N was immobilized into biomass, less than 1% remained in the aqueous phase, and less than 0.03% was protected in minerals. The total N mass flow through each



Figure 5. Concentrations of (a) total living biomass B_{TOT} , (b) phototrophic bacteria B_{PHOTO} , (c) heterotrophic bacteria B_{HET} , and (d) dissimilatory nitrate reducing bacteria B_{DNR} at steady state and for leaching rates $R_{\text{NH}_4^+}$ and $R_{\text{NO}_3^-}$ ranging between 5×10^{-4} and 5×10^{-2} mol \cdot L⁻¹ \cdot day⁻¹. The white areas indicate that the microbial concentration is 0.





Figure 6. Mass fraction of N consumed in (a) phototrophic NH_4^+ assimilation R1, (b) phototrophic NO_3^- assimilation R2, (c) heterotrophic NH_4^+ assimilation R3, (d) heterotrophic NO_3^- assimilation R4, (e) nitrification R5, (f) denitrification R6, (g) dissimilatory nitrate reduction R7, and (h) necromass depolymerization and ammonification R8 at steady state and for leaching rates $R_{NH_4^+}$ and $R_{NO_3^-}$ ranging between 5×10^{-4} and 5×10^{-2} mol $\cdot L^{-1} \cdot day^{-1}$. Note that the contours have values ranging between 0 and 1. The white areas indicate that the N fraction is 0.

microbial reaction at steady state is depicted in Figure 6. The majority of total N was consumed by B_{PHOTO} and B_{HET} through phototrophic NH⁺₄ assimilation in R1 and NEC depolymerization and ammonification in R8, respectively (Figures 6a and 6h). Mineralization of NEC to NH⁺₄ facilitated growth of B_{PHOTO} and B_{HET} , which later contributed to the increase in NEC, therefore resulting in a positive feedback that enabled the ecosystem to self-sustain even in scenarios where nutrient inputs were low. Our analysis shows that NEC depolymerization released NH⁺₄ at a high rate (approximately $2 \times 10^{-2} \cdot \text{mol} \cdot \text{L}^{-1} \cdot \text{day}^{-1}$) in scenarios with low nutrient leaching and was a major contributor to the microbial growth. At high nutrient leaching, inhibition of NEC depolymerization by high availability of $C_6H_{12}O_6$ lowered the concentration of NH⁺₄ available to microbial growth, thus resulting in decreased [B_{TOT}] (Figure 5a). Overall, our results show that NEC depolymerization had a very important contribution to the N cycle.

Analysis in Figure 6 shows that B_{PHOTO} had a higher preference for NH_4^+ over NO_3^- and was mainly synthesized through R1, in line with earlier observations (e.g., Caperon & Meyer, 1972; Cochlan & Harrison, 1991; McCarthy et al., 1977). Although NEC depolymerization played an important role in the N mass flow, B_{HET} synthesized from NEC had lower concentration than that produced by R3 because of smaller biomass yield Y in R8 than in R3 (Table 2). B_{HET} also showed a higher preference for NH_4^+ over NO_3^- ; however, its growth was greatly suppressed by B_{PHOTO} due to high K_M for $C_6H_{12}O_6$. Similar experimental observations were also found



Figure 7. Concentrations of (a) total living biomass B_{TOT} , (b) phototrophic bacteria B_{PHOTO} , (c) heterotrophic bacteria B_{HET} , and (d) dissimilatory nitrate reducing bacteria B_{DNR} at steady state and for leaching rates $R_{\text{NH}_{4}^{+}}$ and $R_{\text{NO}_{3}^{-}}$ ranging between 5×10^{-4} and 5×10^{-2} mol \cdot L⁻¹ \cdot day⁻¹ with $R_{\text{NH}_{4}^{+}}$: $R_{\text{NO}_{3}^{-}}$ = 1:1 and for O₂(aq) saturation ranging from 5 to 100%. The white areas indicate that the microbial concentration is 0.



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Figure 8. Mass fraction of N consumed in (a) phototrophic NH_4^+ assimilation R1, (b) phototrophic NO_3^- assimilation R2, (c) heterotrophic NH_4^+ assimilation R3, (d) heterotrophic NO_3^- assimilation R4, (e) nitrification R5, (f) denitrification R6, (g) dissimilatory nitrate reduction R7, and (h) necromass depolymerization and ammonification R8 at steady state and for leaching rates $R_{NH_4^+}$ and $R_{NO_3^-}$ ranging between 5×10^{-4} and 5×10^{-2} mol $\cdot L^{-1} \cdot day^{-1}$ with $R_{NH_4^+}$ is $R_{NO_3^-} = 1:1$ and for $O_2(aq)$ saturation ranging from 5 to 100%. Note that the contours have values ranging between 0 and 1. The white areas indicate that the N fraction is 0.

in Tufail (1987) and Kirchman and Wheeler (1998). Although $O_2(aq)$ inhibition on B_{DNR} was higher than B_{DEN} , approximately 30% of total N was partitioned into DNR in R7 at high nutrient leaching rates (Figure 6g) because B_{DNR} had lower K_M for both NO_3^- and $C_6H_{12}O_6$ than B_{DEN} .

3.4. Effect of Dissolved Oxygen Content

The reaction network in Figure 2 consisted of both aerobic and anaerobic metabolic processes, which are sensitive to the concentration of dissolved oxygen. To investigate how microbial dynamics and N fluxes are controlled by $[O_2(aq)]$, simulations were conducted for $O_2(aq)$ saturation ranging from 5 to 100%, and for leaching rates $R_{NH_{\pm}^+}$ and $R_{NO_{\pm}^-}$ ranging between 5×10^{-4} and 5×10^{-2} mol \cdot L⁻¹ \cdot day⁻¹ with $R_{NH_{\pm}^+}$: $R_{NO_{\pm}^-} = 1 : 1$.

 B_{TOT} generally increased with increasing $[O_2(aq)]$, but it was not sensitive to $[O_2(aq)]$ when the leaching rates exceeded $3 \times 10^{-2} \cdot \text{mol} \cdot \text{L}^{-1} \cdot \text{day}^{-1}$ (Figure 7a). Interestingly, $[B_{\text{PHOTO}}]$ was highly correlated to $[O_2(aq)]$ (Figure 7b) even though the growth of B_{PHOTO} did not depend on $O_2(aq)$ as a substrate. This is because the NEC depolymerization in R8 was inhibited by low $[O_2(aq)]$, and therefore NH_4^+ available for consumption by B_{PHOTO} decreased with decreasing $[O_2(aq)]$. B_{HET} did not survive well in conditions where $[O_2(aq)]$ was below 50% saturation (Figure 7c), whereas, B_{DNR} could survive in anoxic conditions (Figure 7d). In all tested scenarios, B_{NIT} and B_{DEN} were completely outcompeted by other microbial groups at steady state.

The N mass flow through phototrophic NH_4^+ assimilation in R1 generally decreased with increasing $O_2(aq)$ saturation (Figure 8a), while the N fraction consumed by NO_3^- phototrophic assimilation in R2 increased with increasing $[O_2(aq)]$ at high nutrient leaching rates (Figure 8b). A small fraction of N was partitioned into heterotrophic metabolism in R3 and R4 at low leaching rates, while they were not active in low $[O_2(aq)]$ and high leaching rates (Figures 8c and 8d). Approximately 30% of N was consumed by B_{DNR} in R7 in low $[O_2(aq)]$ regardless of leaching rates (Figure 8g). The N fraction consumed in NEC depolymerization in R8 increased with increasing $O_2(aq)$ saturation, but the reactions was inhibited at high nutrient conditions (Figure 8h).

4. Discussion

The microbial functional groups described in the reaction network (Figure 2) included different microbial species that performed similar ecological functions, hence assuming that members of the same group were equipped with the same or similar enzymes for the same metabolic mechanisms; in fact, no significant variation was found in K_M when experiments were conducted with different microbial species of the same functional group (Caperon & Meyer, 1972). Several studies also showed that K_M values may greatly depend



on the ambient nutrient concentrations of the original habitat (e.g., Caperon & Meyer, 1972; MacIsaac & Dugdale, 1969); for instance, phytoplankton populations obtained from eutrophic ecosystems were observed to have much higher K_M values for NO₂ as compared to those living in oligotrophic ecosystems (MacIsaac & Dugdale, 1969). The microbial communities used to inoculate sediment mixtures in this study were sampled from an estuary that has relatively high $[NH_{4}^{+}]$ and $[NO_{2}^{-}]$ (approximately 1.2 mM of $[NH_{4}^{+}]$ and 6.6 mM of [NO₂]), and hence, the parameters calibrated here may reflect only the metabolic characteristics of microorganisms adapted to high nutrient concentrations and may not be applicable to ecosystem where nutrients are strongly limiting. Along this line, the capability of microorganisms to adapt to a specific nutrient condition (Eppley & Coatsworth, 1968) was not accounted for in the model, and we assumed that enzymes responsible for metabolism were not altered after long-term presence in such an environment. We note also that nitrification pathway in R5 involves two processes conducted separately by ammonia-oxidizing bacteria and archaea, and nitrite-oxidizing bacteria, which may have different substrate affinities, yields, and sensitivities to environmental conditions such as temperature and oxygen content (e.g., Dang & Chen, 2017; Kits et al., 2017). Because concentration of NO_{2}^{-} was not measured, experiments were unable to give sufficient constraint for retrieving the kinetic parameters of these two intermediate processes separately; hence, these two processes (ammonia and nitrite oxidation) were treated here as one reaction mediated by one microbial functional group.

Microorganisms were found to attach on SPM at a few orders of magnitude higher concentration than those living freely in ambient water (e.g., Caron et al., 1986; Turley & Mackie, 1994). These two groups of microorganisms were not differentiated in the mode, and hence, the estimated parameters reflected the combined effects resulting from metabolism of both aggregate-attached and free-living microorganisms; however, we note that aggregate-attached bacteria may have higher enzymatic activity and reaction rate than free-living bacteria as evident in Goulder (1977) and Grossart et al. (2007). Several studies also observed the grazing of aggregate-attached microorganisms by heterotrophic microflagellates and suggested that the abundance of bacteria living attached to SPM was controlled by heterotrophic grazing (e.g., Caron, 1987; Kiørboe et al., 2004). Although we note that antagonistic relationships such as predation, grazing, scavenging, and inhibition by metabolites of other species occur among microbial communities (e.g., Cole, 1982; Guerrero et al., 1986; Pernthaler, 2005), these interactions were not explicitly included in the model; indeed, we assume that these interactions were implicitly accounted for through mortality.

Although microorganisms may grow better in environments where micronutrients are available (MacIsaac & Dugdale, 1969), experiments herein were conducted with only inorganic N (NH₄⁺ and NO₃⁻) and C₆H₁₂O₆ without accounting for other macronutrients and micronutrients. Because sulfur-based compounds were not added to the test samples, chemolithoautotrophic denitrification that uses sulfur as electron donor (Batchelor & Lawrence, 1978) was not included in the reaction network. NO₂⁻, on the other hand, was very likely present in the test samples because it is an intermediate product of nitrification in R5 and denitrification in R6. Anaerobic ammonium oxidation (Anammox) that uses NO₂⁻ as electron acceptor (e.g., Dalsgaard et al., 2005) was, however, not considered in the reaction network because experiments described above were conducted in oxic conditions, while Anammox bacteria has high sensitivity to oxygen inhibition (e.g., Davies et al., 1989; Kalvelage et al., 2011); thus, Anammox was assumed to be negligible in our case. We note also that N₂-fixing microorganisms may have a contribution to the N cycle (e.g., Howarth et al., 1988; Newell et al., 2016); however, N₂ fixation was not measured in our experiments and its effect was not included in the reaction network.

Temperature has been reported in the literature as one of the factors that alters the enzymatic activities of microorganisms (e.g., Maggi & Riley, 2017; Toseland et al., 2013). For instance, microbial affinity for NO_3^- in phototrophic and heterotrophic assimilation was found to decrease with decreasing temperature (Reay et al., 1999), whereas a reduction in ammonia oxidation and denitrification rates were also observed as temperature decreased (e.g., Saleh-Lakha et al., 2009; Tourna et al., 2008; Wang et al., 2015). Apart from biochemical reactions, chemical adsorption on clay is also sensitive to temperature (Almeida et al., 2009). In this study, temperature in both experiments and model was kept constant at 21°C, and hence, the parameters calibrated here reflected only the microbial metabolism and adsorption kinetics specific to that temperature.

The model considered a comprehensive ecological feedback loop that explicitly accounted for the biomass of different functional groups and the necromass, which are not normally included in most aquatic biogeochemical models (Robson, 2014). Some models did consider explicitly the biomass with one or more



functional groups; however, most of these models focused on biogeochemical processes (e.g., Allen & Clarke, 2007; Kaufman & Borrett, 2010) with little emphasis on the dynamics of microbial diversity (e.g., Bruce et al., 2006; Prokopkin et al., 2010). Although the calibrated parameters were specific to the microbial strains and environmental conditions tested here, the reaction network and model structure presented herein provide a modeling framework that could be applied to predict, monitor, and manage water quality and microbial communities, not only in natural aquatic ecosystems but also in engineered environments such as wastewater treatment plants, bioremediation plants, bioreactors, aquaculture farms, and microalgae cultivation plants.

4.1. Conclusions

The role of microorganisms in controlling the N cycle in a sediment suspension was investigated by integrating experiments with a biogeochemical model that considers abiotic and biotic processes including chemical adsorption on minerals, aqueous complexation, gas dissolution, microbial metabolism, and necromass dynamics. Biomass was described explicitly in the model with five microbial functional groups and eight different microbial metabolic pathways of inorganic N were accounted for in an ecological feedback loop involving competition and facilitation interrelationships. The model was calibrated and validated against six experiments and captured relatively well the dynamics of N, with 95% of validation tests passing the goodness-of-fit benchmark. In steady state analyses, phototrophic microorganisms appeared to survive competition and dominated the ecosystem in all nutrient leaching scenarios. The competitive and facilitative interactions between microbial functional groups were susceptible to nutrient leaching and the concentrations of dissolved oxygen. For example, heterotrophic microorganisms were outcompeted by phototrophs at high nutrient leaching rates and low $O_2(aq)$ concentration, while both phototrophs and heterotrophs coexisted in facilitative relationship in low nutrient and oxic conditions with heterotrophs providing NH $_4^4$ to phototrophs through the necromass depolymerization process. Our simulation results show that necromass depolymerization played a very major role in governing the dynamics of sedimentary microbial community and the N cycle.

Notation

Anammox Anaerobic ammonia oxidation.

- B_{DEN} Denitrifying bacteria.
- B_{DNR} Dissimilatory nitrate reducing bacteria.
- B_{HET} Heterotrophic bacteria.
- $B_{\rm NIT}$ Nitrifying bacteria.
- B_{PHOTO} Phototrophic bacteria.
 - B_{TOT} Total living bacteria.
 - DNR Dissimilatory nitrate reduction.
 - IA Index of agreement.
- NABA Nutrient and biomass affected.
- NABF Nutrient affected and biomass free.
- NEC Necromass.
- NFBF Nutrient and biomass free.
- NRMSE Normalized root-mean-square error.
 - NOB Nitrite-oxidizing bacteria.
 - NSE Nash-Sutcliffe efficiency.
- PBIAS Percent bias.
 - R Correlation coefficient.
 - SPM Suspended particulate matter.

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